Photocatalytic Hydrogen Production from Water with Nonfood Hydrocarbons as Oxidizing Sacrifice Agents

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To enhance photocatalytic water splitting, various oxidizing sacrifice agents (OSA) have been added to the system in order to scavenge the coproduced O_2 , and, thus, to hinder the reverse reactions. In the aim of achieving carbon-neutral photocatalytic water splitting, nonfood hydrocarbons of castor- and jojoba-oils were evaluated as OSA. Moreover, various surfactants were tested as emulsifiers for W/O binary solution for promoting photocatalytic water splitting rate. Among the OSA used, the castor-oil was found to be more suitable candidate compared to jojoba-oil, which was attributed to its smaller carbon chain numbers of mainly 18. Without surfactants, around 20 vol %-castor-oil aqueous binary solution with $TiO_2/Pt(0.10 \text{ wt \%})$ provided the highest water splitting rate of about 30 mL- $H_2/(m^2 \cdot h)$. Among tested surfactants, liquid-detergent was the best due to its optical transparency. 40 vol %- or 60 vol %-castor-oil emulsion with a drop of liquid-detergent resulted in a water splitting rate of 125 mL- $H_2/(m^2 \cdot h)$, which was four times greater that the aforementioned highest value. © 2010 American Institute of Chemical Engineers AIChE J, 57: 2237–2243, 2011

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Introduction

The recent increase in energy demand could soon lead to a disruption in energy supply caused by various factors including the exhaustion of fossil fuels. Hence, the alternative energy sources such as fuel cells are being developed, and there utilization might soon result in a society based on H₂ energy the World Energy Network (WE-NET) project in the period from 1993–2003 provided a great deal of credits on the basic policy of H₂ production by water electrolysis

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using electric-power generated from renewable energy sources such as hydropower and windpower. $^{1-3}$ Despite this fact, present H_2 production still relies on thermochemical conversion of fossil fuels, due to the supply/demand mismatches in terms of time, place, quantity and quality. $^{4-9}$

According to WE-NET, ¹⁰ the electrochemical reactions play important roles in H₂ production, and photoelectrochemical reaction known as Honda/Fujishima effect, based on splitting water by Pt/TiO₂ with ultraviolet rays, is of great importance. ^{11–13} To promote photocatalytic water splitting rates, various oxidizing sacrifice agents (OSA) have been added to water. The role of OSA is to scavenge the coproduced O₂ due to water splitting, and, thus, to prevent the reverse reaction of O₂ with H₂ to H₂O from occurring. ^{14–21} Typically, the OSA are

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Table 1. Properties of OSA and Surfactant Candidates

OSA	main components	s number of carbon in a mole	cule solubility to water	color	principal utilizations
	ricinoleic acid	18	insoluble	transparent	lubricant purgative
	oleic acid	18		_	
	linoleic acid	18			
jojoba-oil	eicosenoic acid	20	insoluble	transparent	cosmetics lubricant
	erucic acid	22			
	amylose	20000-85000	soluble to hot water	transparent	food
	amylopectin	60000-1700000			
surfactant		natural or artificial	solubility to water	color	cost
lecithin		natural	insoluble	orange	expensive
saponin		natural	insoluble	orange	expensive
liquid detergent		artificial	soluble	transparent	very cheap

eatable hydrocarbons such as saccharides, alcohol and acetic acid, but the use of nonfood OSA such as cellulose, benzoic acids and pyroligneous acid has also been reported. 15,18,22 Given this, saccharides and acetic acid were the preferred OSA in our recent study.²²

However, the continuing rumors on the possible worldwide food crisis should also be taken into consideration, and, hence, the authors decided to shift attentions to natural nonfood hydrocarbons such as castor-oil and jojoba-oil, which could be used for carbon-neutral photocatalytic water splitting. Unfortunately, these OSA candidates are known to be water-insoluble, and, hence, lower water splitting rates are to be expected due to small W/O (water/oil) interface area in binary mixtures. Assuming that higher water splitting rates can be obtained by altering W/O binary solutions to stabilized emulsified solutions characterized by higher W/O interface areas, the authors had also surveyed natural surfactants such as lecithin and saponin. Tables 1 shows the properties of natural nonfood OSA and surfactant candidates. Starch with extremely high-molecular-weight and soluble in hotwater was selected for optimization of TiO₂/Pt powders. The starch had similar proprieties as natural nonfood OSA candidates but water-soluble; this may lead to a simpler discussion of the obtained results. As a referential surfactant, a commercial liquid-detergent with higher availability was selected because of its extremely low cost.

In this study, optimizations of TiO₂/Pt powders were done at first using starch aqueous solution. Then, the optimized TiO₂/Pt powders were used to assess the feasibility of photocatalytic water splitting from various W/O binary solutions, and to determine the best-performing OSA candidate shown in Table 1. Subsequently, photocatalytic water splitting from W/O emulsified solutions containing a surfactant in Table 1 was carried out in order to clarify the best mixture. Finally, future strategies for the photocatalytic water splitting from W/O emulsified solutions leading to the practical stage applications were declared.

Experimental apparatus and procedures

Figure 1 shows a schematic drawing of the experimental apparatus. Main reactor was made of Pyrex glass in cylindrical shape of 90 mm internal diameter and 40 mm tall, having about 255 mL in volume. The cylinder had two taps for replacing air inside by Ar in order to obtain higher H₂ producing rates²² and to allow gas-sampling. The top cover was made of solid quartz glass with high transmissivity toward ultraviolet rays. To maintain a constant reaction temperature, a cooling chamber made of Pyrex glass was attached to the bottom of the cylinder, where water at 293 K was circulated throughout the whole experimental period. Since H₂ producing efficiency by water electrolysis is quite high above 95%, the cooling system in the practical application stage should be replaced by radiating fins or other systems consuming no electricity. In the same way, other electrical equipments such as magnetic stirring and temperature monitoring were excluded in the apparatus, imitating the practical operations as much as possible.

TiO₂ powders utilized were P25 (a mixture of 70 mol %anatase form and 30 mol %-rutile form) produced by Nippon Aerosil Co., Ltd. The P25 indicated superior H2 producing efficiencies comparing to other commercial products used in our former studies such as famous ST01 produced by Ishihara Sangyo Kaisha, Ltd., and reagents purchased from Wako Pure Chemical Industries, Ltd., in our former studies. 22-24 Next, Pt loading to TiO2 powders was performed by photodecomposition of hexachloroplatinic acid.²⁵ Almost the same-size distribution of TiO2/Pt powders could be obtained owing to powder grinding for sufficiently longer times of more than 60 min in an automatic grinder (ANM1000, Nitto Kagaku Co., Ltd.), independent to TiO2 type and loaded Pt wt % content up to 0.50. Figure 2 shows a representative particle-size distribution of P25 with 0.10 wt %-Pt loaded, which was measured by a laser diffraction particle-size analyzer (LA-920, Horiba, Ltd.).

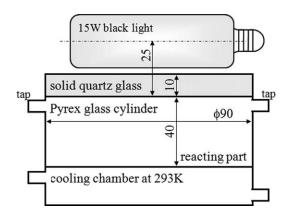


Figure 1. Schematic drawing of experimental apparatus.

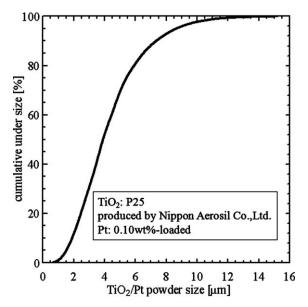


Figure 2. Particle size of TiO₂/Pt powders.

Regarding the water splitting experiments, W/O binary solution of 5.0 mL and/or the surfactant prepared in advance according to Table 1 was poured into the reactor along with the TiO₂/Pt powders. Then, the whole apparatus was manually agitated to replace air inside by Ar. Then, after starting the circulation of water (293 K) in the cooling chamber, the light irradiation by 15.0 W black light (EFD15BLB-T, Toshiba Lighting and Technology Corp.) was initiated. The light intensity stated in the catalog is 1.30 W in the ultraviolet region. Finally, H₂ concentration inside the gas phase of reactor was measured by means of TCD gas-chromatography (GC-8A, Shimadzu Corp.). In these procedures, experimental repeatabilities can be conveniently preserved.

Results and Discussion

Optimal TiO₂/Pt powders

Figure 3 shows the H₂ producing rates obtained with various amounts of TiO₂/Pt(0.10 wt %) from starch aqueous solution of 25 g/L. It can be seen that no water splits were obtained without TiO₂/Pt powders, and, thus, there was no H₂ produced by ultraviolet decomposition. Furthermore, when the experiments were carried out in the presence of TiO₂/Pt powder, H₂ generation was clearly observed, and H₂ producing rate was observed to steeply increase with an amount of TiO₂/Pt powders up to around 0.5 g. Above this content, the H₂ producing rate seemed to attain a constant value, which was attributed to plane surface reactions in this system without flowing fluids and solids. Hence, 0.50 g of TiO₂/Pt powders was used as an optimum dosage in the subsequent experiments.

Figure 4 shows H₂ producing rates for different Pt wt % loaded to TiO₂ powders. No water splitting by only TiO₂ indicated that Pt plays an important role of capturing excited electrons, so called Schottky effect. It can be seen that H₂ producing rate increased proportionally to Pt wt % up to about 0.1, and then decreased. This may have resulted from change in Pt dispersing condition as illustrated in the bottom

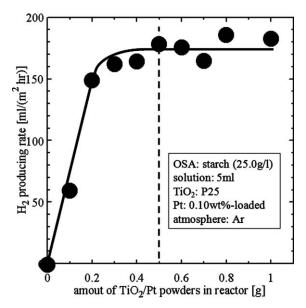


Figure 3. Optimal amount of TiO₂ powders.

part of this figure. It is well-known that Pt itself has no photocatalytic functions, but can be a catalyst for recoupling of produced H_2 and O_2 to water, so that the extensive amount of Pt resulted in the deterioration of H_2 producing rate. Consequently, the optimum Pt wt % loaded to TiO_2 powders was revealed to be around 0.1 wt %, and this optimum was used for further experiments.

Feasibility of H_2 production from W/O binary solutions

Figure 5 shows time trends of H_2 production from binary solutions of water and castor- or jojoba-oil. First of all, it is found that H_2 can be produced from such heterogeneous W/O binary solutions, concluding that oils can become OSA for photocatalytic water splitting. It is clear that castor-oil is better than jojoba-oil as OSA, resulting from their different

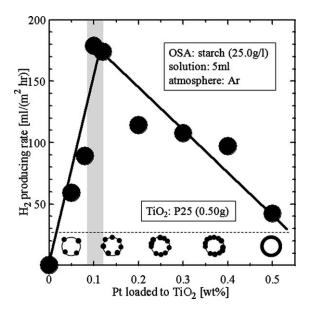


Figure 4. Optimum Pt wt % loaded to TiO₂ powders.

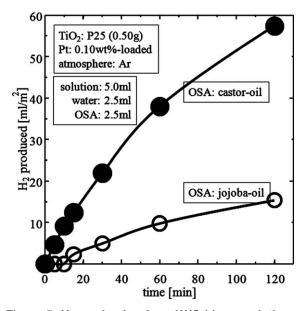


Figure 5. H₂ production from W/O binary solutions.

carbon chain numbers in Table 1. Therefore, castor-oil is used in latter experiments.

H_2 production from binary solutions of water/castor-Oil

Figure 6 shows H_2 producing rates for various concentrations of castor-oil to water. The most notable point is that H_2 was produced from 100 vol %-castor-oil, i.e., photocatalytic decomposition of castor-oil took place. It is reasonable to assume that the contribution of castor-oil decomposition to the whole H_2 production was directly proportional to its concentration, and such an assumption is represented by the triangulated gray area in this figure. The gray area, thus, corresponds to H_2 produced by direct photocatalytic decomposition of castor-oil itself.

In order to discuss the roles of castor-oil as OSA, the triangulated area was subtracted from Figure 6, resulting in a fine symmetric curve as shown in Figure 7, representing H₂ producing rate by photocatalytic water splitting. To provide clear explanations, a simple illustration based on our observation was added to Figure 7. First, up to 30 vol % of castor-oil, H2 producing rate was found to increase and it was also noticed that the castor-oil floated on the water surface in the form of droplets. Given the fact that the water splitting takes place at W/O interface, the H₂ producing rate increase was attributed to an increase in W/O interface area. Second, at castor-oil concentrations above 30%, the water surface was completely covered with castor-oil, which resulted in a constant W/O interface area. The thickness of the surface layer of castor-oil grew with the castor-oil concentration, and the decline in H2 producing rate was most likely caused by absorption of ultraviolet rays by the castoroil layer and the consequent deterioration in the optical intensity of ultraviolet rays at W/O interface.

Consequently, as long as the oils are utilized as OSA, further expansion of W/O interface area is necessary to bring this system up to a practical stage. Typical ways to enlarge the W/O interface area are mechanical agitations and

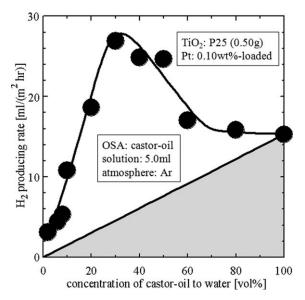


Figure 6. H₂ production from water and castor-oil binary solutions in various concentrations.

enforced convections using magnetic stirrers. However, since water electrolysis is known to be efficient above 95%, expansion of W/O interface area must be realized without any electric devices. Therefore, W/O emulsification using surfactants was adopted in the next section.

H_2 production from water/castor-oil emulsions with various surfactants

Figure 8 shows time plots of H_2 production from water/20 wt %-castor-oil emulsions with about 0.1 g of various surfactants in Table 1. In these experiments, a commercially available liquid-detergent was used, and its water content was determined using a thermogravimetric analysis (TGA-50H, Shimadzu Corp.). Subsequently, the water content in

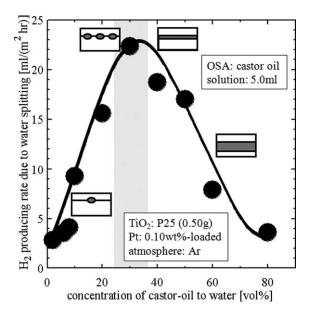


Figure 7. H₂ production by photocatalytic water splitting with castor-oil as OSA.

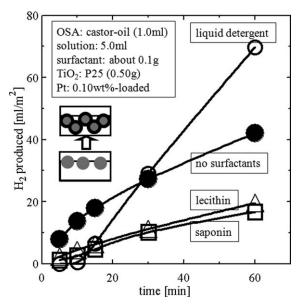


Figure 8. H₂ production from water and castor-oil emulsions with various surfactants.

the liquid-detergent was found to be 33 wt %, and the dosage of liquid-detergent was corrected accordingly First, it can be seen that H₂ productions from W/O emulsions at the beginning of the experiments were low and without exceptions, comparing with the binary solution. This fact indicates that the surfactants utilized in this study are all improper as OSA. After a while, better H₂ productions were obtained. Such transitions are completely opposite to the cases of W/O binary solutions, leading from finer castor-oil drops fully coated by surfactants as illustrated in this figure. In other words, unsuitable surfactants play roles as OSA and hardly decompose photocatalytically at the beginning, and then higher W/O interface areas contribute H₂ production.

Among tested surfactants, only the liquid-detergent can promote water splitting, compared to W/O binary case. Although other natural surfactants of lecithin and saponin can also stabilize W/O emulsions, no promoting effect for water splitting was attributed to their colorations in orange, which must absorb ultraviolet rays at only upper regions of the W/O emulsions. Therefore, it can be concluded that W/O emulsification using optical transparent surfactants has predominance for photocatalytic H₂ production.

Optimal emulsion of water/castor-oil/liquid-detergent

Figure 9 shows H₂ producing rates from various water/ castor-oil/liquid-detergent emulsions. It can be seen that the optimal dosage of liquid-detergent varied with the castor-oil concentrations. This might have resulted form three contraeffects by liquid-detergent; namely expansion of W/O interface area, impropriety as OSA and difficulty for photocatalytic decomposition. H₂ producing rates could be enhanced by adding suitable amount of liquid-detergent to any W/O solutions, up to about four times of respective W/O binary cases. The best H₂ producing rate was acquired from 40 vol %-castor-oil with a drop of liquid-detergent, and almost the same rate was seen from 60 vol %. This fact indicated that

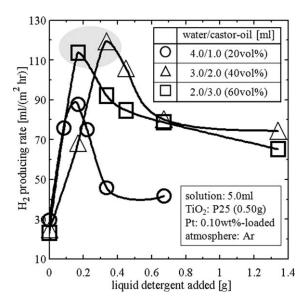


Figure 9. H₂ production from various ratios of water/ castor-oil/liquid-detergent emulsions.

W/O emulsified systems suited a wide-range of W/O ratios, compared with the binary systems.

Since the best H₂ producing rate of about 120 mL-H₂/ (m²·h) from W/O emulsified system is almost the same as that from homogeneous starch aqueous solution of about 175 mL-H₂/(m²·h) in its maximum. Therefore, it can be concluded that liquid-detergent provides a great help to make W/O system homogeneous.

Tip trial of newly developed TiO₂ named P90 by Nippon Aerosil Co., Ltd.

Recently, Nippon Aerosil Co., Ltd. has developed new TiO₂ powders named P90. Figure 10 shows time plots of H₂ production from binary 20 vol %-castor-oil solution by P90

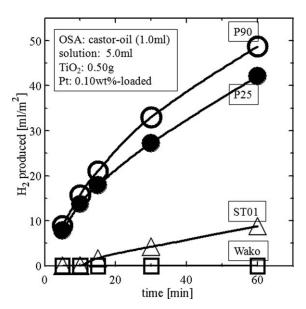


Figure 10. Best TiO₂ powders.

together with ST01, reagent by Wako and P25. As expected, it is seen that ST01 and reagent by Wako were less efficient for water splitting than P25. The most noteworthy is that P90 had a superior $\rm H_2$ producing capacity of more than 15% compared to P25.

Energy converting efficiency and future strategies

The best H₂ producing rate of 120 mL-H₂/(m²·h) was obtained from water/40 vol %-castor-oil/liquid-detergent-drop emulsified systems. P90 must raise this best value 15% at least, leading to 138 mL-H₂/(m²·h). Here, light energy to the reactor from the black light was about 0.6 W, which was a half of the value stated in the catalog. Taking H₂ energy density of 12.8MJ/m³ into consideration, energy converting efficiency was calculated to be about 0.52%. To increase the energy converting efficiency, the following future strategies are of outmost importance.

First, concerning material strategies, so far only limited numbers of nonfood natural hydrocarbons were tested as OSA, but the tests should be extended toward many other OSA candidates such as humins and terpenes. Similarly, various studies have shown the importance of the selection of TiO₂ powders, and there are many commercially available TiO₂ powders such as Fuji Titanium Industry Co., Ltd., Tayca Corp., and Titan Kogyo, Ltd. Furthermore, the tailormade TiO2 powder in nano-orders could also bring an enormous improvement, especially by building-up method of spray pyrolysis. 26,27 Additionally, the authors have recently developed new technology of salt-added super- or subcritical fluid annealing processes that could improve crystallinity of fine metallic powders with restricting their agglomerations.²⁸ Using this process, TiO₂ powders without lattice defects could be easily obtained. In summary, screening experiments could result in a significant rise in energy converting efficiency drastically.

Secondary, concerning hydrodynamic strategies, the authors have focused on Rayleigh-Benard convection to obtain a medium flow without consuming electricity. Such a medium flow can provoke present plane surface photocatalytic reaction to volumetric one. The authors have already confirmed about thrice as high H₂ producing rate due to Rayleigh-Benard convection induced by waste heats, and our optimizing works in progress are expected to bring about a remarkable promotion of the energy converting efficiency.

Finally, other strategies are related to chemical and process engineering. For example, precise control of pH value, ²² H₂ separation by semipermeable membranes and adding O₂ absorbents such as Ageless produced by Mitsubishi Gas Chemical Co., Inc., could also contribute to an improvement in energy converting efficiency eminently.

Conclusions

As oxidizing sacrifice agents for photocatalytic water splitting, nonfood natural hydrocarbons of castor- and jojoba-oils were evaluated in order to establish a genuine carbon-neutral H_2 producing process. It can be concluded that castor-oil with smaller carbon chains of mainly 18 was better than jojoba-oil with longer carbon chains of mainly 20 and 22. The highest H_2 producing rate of 30 mL- $H_2/(m^2 \cdot h)$ was obtained from 20 vol %-castor-oil binary solution. Further-

more, various surfactants were used to emulsify the W/O binary solution, and the optical transparency of these surfactants was found to be critical. In accordance with these findings, 40 vol %-castor-oil emulsified solution with a drop of transparent liquid-detergent gave the best water splitting rate, which was about four times greater than the highest value in W/O binary case.

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Literature Cited

- Hijikata T. Research and development of international clean energy network using hydrogen energy (WE-NET). Int J Hydrogen Energy. 2002;27:115–129.
- Iwasaki W. A consideration of power density and hydrogen production and utilization technologies. *Int J Hydrogen Energy*. 2003;28: 1325–1332.
- 3. Chiba M, Arai H, Fukuda K. WE-NET: Japanese hydrogen program. *Int J Hydrogen Energy*. 1998;23:159–166.
- Cui W, Feng L, Xu C, Lue S, Qui F. Hydrogen production by photocatalytic decomposition of methanol gas on Pt/TiO₂ nano-film. Cat Comm. 2004;5:533–536.
- Pedrero CM, Cellier C, Ruiz P. Rh/Ti-SiO₂ catalysts prepared by organic grafting: A novel class of catalysts towards hydrogen production by partial oxidation of methane. *Catal Today*. 2006;117: 362–368.
- Perkas N, Zhong Z, Chen L, Besson M, Gedanken A. Sonochemically prepared high dispersed Ru/TiO₂ mesoporous catalyst for partial oxidation of methane to syngas. *Catal Let*. 2005;103:9–14.
- 7. Song C. Recent advances in catalysis for hydrogen production and fuel processing for fuel cells. *Catal Today*. 2008;49:1–3.
- Wu T, Yan Q, Wan H. Partial oxidation of methane to hydrogen and carbon monoxide over a Ni/TiO₂ catalyst. J Mol Cat A Chem. 2005;226:41–48.
- Yoshida H, Hirao K, Nishimoto J, Shimura K, Kato S, Itoh H, Hattori T. Hydrogen production from methane and water on platinum loaded titanium oxide photocatalysts. *Phys Chem C*. 2008;112: 5542–5551.
- Anantharaman V, Pintauro PN. The electrocatalytic hydrogenation of glucose: kinetics of hydrogen evolution and glucose hydrogenation on raney nickel powder. *J Electrochem Soc.* 1994;141: 2729–2741.
- Fujishima A, Honda K. Electrochemical photolysis of water at a semiconductor electrode. Lett Nature. 1972;238:37–38.
- Kitano M, Tsujimaru K, Anpo M. Hydrogen production using highly active titanium oxide-based photocatalysts. *Topics Cat.* 2008;49:4–17.
- Sato S, White JM. Photo assisted hydrogen production from titanium and water. J Phys Chem. 1981;85:592–594.
- 14. Fu X, Long J, Wang X, Leung DY, Ding Z, Wu L, Zhang Z, Li Z, Fu X. Photocatalytic reforming of biomass: A systematic study of hydrogen evolution from glucose solution. *Int J Hydrogen Energy*. 2008;33:1–8.
- Kawai T, Sakata T. Conversion of carbonhydrate into hydrogen fuel by a photocatalytic process. *Nature*. 1980;286:474

 –476.
- Matsuoka M, Kitano M, Takeuchi M, Tsujimaru K, Anpo M, Thomas JM. Photocatalysis for new energy production: Recent advances in photocatalytic water splitting reactions for hydrogen production. *Catal Today*. 2007;122:51–61.
- Nada AA, Hamed HA, Barakat MH, Mohamed NR, Veziroglu TN. Enhancement of photocatalytic hydrogen production rate using photosensitized TiO₂/RuO₂-MV²⁺. *Int J Hydrogen Energy*. 2008;33: 3264–3269.

- Nosaka AY, Nishino J, Fujiwara T, Ikegami T, Yagi H, Akutsu H, Nosaka Y. Effects of thermal treatments on the recovery of adsorbed water and photocatalytic activities of TiO₂ photocatalytic systems. J Phys Chem B. 2006;110:8380–8385.
- Sato S. Photo-Kolbe reaction at gas-solid interfaces. J Phys Chem. 1983;87:3531–3537.
- Strataki N, Bekiari V, Kondarides DI, Lianos P. Hydrogen production by photocatalytic alcohol reforming employing highly efficient nanocrystalline titania films. *App Cat B*. 2007;77:184–189.
- Zielinska B, Palen EB, Kalenczuk RJ. Photocatalytic hydrogen generation over alkaline-earth titanates in the presence of electron donors. *Int J Hydrogen Energy*. 2008;33:1797–1802.
- Deguchi S, Shibata N, Takeichi T, Furukawa Y, Isu N. Photocatalytic hydrogen production from aqueous solution of various oxidizing sacrifice agents. *J Jpn Petro Inst*. 2010;53:95–100.
- Sugiura Y, Deguchi S. Rate enhancement of photocatalytic water decontamination with dispersed light source of ultraviolet-electroluminescence powders. *Int Sym EcoTopia Sci.* 2007.

- 24. Deguchi S, Kobayashi N, Sugiura Y, Katsuki R. Rate enhancement of photocatalytic degradation with nonlinear optic effects and/or visible light phosphors. Presented at: Fifth International Conference on Unsteady-State Processes in Catalysis; November 2006; Osaka, Japan; pp. 187–188
- Sato S, White JM. Photoassisted water-gas shift reaction over platinized titanium dioxide catalysts. J Am Chem Soc. 1980;102:7206– 7210.
- Deguchi S, Hasatani M, Kobayashi N. Formation mechanism of TiO₂ fine particles prepared by the spray pyrolysis method. *Drying Tech.* 1994;12:577–591.
- Deguchi S, Hasatani M, Kobayashi N. Preparation of fine particles of metal-metal oxide semiconductors by spray pyrolysis method. Kagaku Kogaku Ronbunshu. 199420:529–534.
- Deguchi S, Ogawa M. Thermal treatment method of particulate metal-compounds. Japenese patent 2010–072988. 2010.

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